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Comparison of Microwave, Ultrasound and Accelerated-Assisted Solvent Extraction for Recovery of Polyphenols from *Citrus Sinensis* Peels

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1	Full title:
2	Comparison of Microwave, Ultrasound and Accelerated-Assisted Solvent Extraction for
3	Recovery of Polyphenols from <i>Citrus Sinensis</i> Peels
4	Running title:
5	Comparison of extraction methods for Polyphenols from <i>Citrus</i> Peels
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19 Abstract

P C C F K

20	Peel of Citrus sinensis contains significant amounts of bioactive polyphenols that
21	could be used as ingredients for a number of value-added products with health benefits.
22	Extraction of polyphenols from the peels was performed using a microwave-assisted
23	extraction (MAE) technique. The effects of aqueous acetone concentration, microwave
24	power, extraction time and solvent-to-solid ratio on the total phenolic content (TPC), total
25	antioxidant activity (TAA) (using DPPH and ORAC-values) and individual phenolic acids
26	(IPA) were investigated using a response surface method. The TPC, TAA and IPA of peel
27	extracts using MAE was compared with conventional, ultrasound-assisted and accelerated
28	solvent extraction. The maximum predicted TPC under the optimal MAE conditions (51%
29	acetone concentration in water (v/v), 500 W microwave power, 122 s extraction time and 25
30	mL g^{-1} solvent to solid ratio), was 12.20 mg GAE g^{-1} DW. The TPC and TAA in MAE
31	extracts were higher than the other three extracts.

Keywords: *Citrus sinensis*; microwave extraction; ultrasound extraction; accelerated solvent
 extraction, phenolic compounds; antioxidant activity; response surface method

34 1. Introduction

35 Citrus is one of the most important fruit crops in the world. Production of citrus fruits 36 has increased enormously in the last few decades, going from an average of 62 million tons a 37 year in the period 1987-1989 to about 100 million tons in the year 2010 (Food and 38 Agriculture Organization, 2014). Citrus is grown in more than 100 countries all over the 39 world, mainly in tropical and subtropical areas, where favorable soil and climatic conditions 40 prevail for citrus cultivation. Citrus fruits are marketed mainly as fresh fruit or as processed 41 juice. During processing of citrus fruits, huge amount of peels are generated as by-product, 42 which do not add value to the product as these are discarded or dumped. Potential use of citrus peels as value-added products has been widely studied because it contains numerous 43 44 biologically active compounds including natural antioxidants such as phenolic compounds (Hayat, Hussain, Abbas, Farooq, Ding, Xia, et al., 2009). Citrus phenolics have been the 45 46 subject of increased interest in the last few years because of their contributions to the quality attributes with color, bitterness, astringency, antioxidant activity and flavor (Legua, Forner, 47 Hernández, & Forner-Giner, 2014). In recent years, the physiological function of foods 48 49 including fruits, vegetables, legumes and grains, and food components such as 50 phytochemicals has received much attention. Possible correlations between the biologically 51 active compounds and human health have generated interest in *in-vitro* and *in-vivo* studies. 52 Phenolic compounds are a major class of phytochemicals found in plants and consist of a 53 large variety of derivatives including simple phenols, phenylpropanoids, benzoic acid 54 derivatives, flavonoids, tannins, lignans and lignins. These compounds have diverse 55 properties as antioxidants, anti-inflammatory, anti-allergic, and ant-carcinogenic activity, and 56 these properties improve the quality and value of the food (Liu, 2004). The antioxidant 57 property is associated with the ability of the phenolic compounds to scavenge free radicals, 58 break radical chain reactions and chelate metals. It was also found that the phenolic

59 compounds inhibit human immunodeficiency viral replication (HIV), human simplex virus 60 (HSV), glucosyl transferases of *Streptococcus mutans* (dental carries), ascorbate auto-61 oxidation (green tea), cytotoxic effects, tumor promotion and xanthine and monoamine 62 oxidases (Proestos, Boziaris, Nychas, & Komaitis, 2006). 63 Phytochemicals from the citrus peels could add value to the citrus processing industry when the compounds are extracted effectively by applying efficient extraction technologies. 64 65 Optimization and standardization of extraction parameters for these health benefitting 66 bioactive phytochemicals from citrus peels are important to retain their antioxidative properties. Application of various techniques for sample preparation and processing of 67 68 bioactive compounds from plant materials have been reviewed by many researchers (Chumnanpaisont, Niamnuy, & Devahastin, 2014; Fernández-Agulló, Freire, Antorrena, 69 70 Pereira, & González-Álvarez, 2013). The first step of processing is "extraction", which 71 involves separation of phytochemicals from the cellular matrix of citrus peel. There are 72 various methods for extracting phenolic compounds such as leaching-out extraction (Zhang, Bi, & Liu, 2007). Generally, extraction is being carried out using conventional technologies 73 such as solvent extraction (liquid-liquid and solid-liquid extraction) by assistance of external 74 75 factors (e.g. mechanical agitation, pressing, or heating systems). The "ideal" extraction method must provide high extraction rates and should be non-76 destructive and time saving (Rombaut et al., 2014). In addition, as per the environmental 77 78 requirements and economic impact, the food and nutraceutical industry prefer green 79 extraction and processing to ensure a safe and high quality extract/product (Chemat, Vian, & 80 Cravotto, 2012). Recently, more rapid and automated methods including supercritical fluid 81 extraction (SFE), pressurized liquid extraction (PLE) or microwave-assisted extraction

82 (MAE), ultrasound extraction (UAE) and accelerated solvent extractor (ASE) have been used

83 (Krishnaswamy, Orsat, Gariépy, & Thangavel, 2013; Périno-Issartier, Zill-e, Abert-Vian, &

84 Chemat, 2011). The above extraction methods are advantageous compared to conventional 85 methods because they can be carried out in the absence of light and oxygen, cope with the 86 demand for a reduction in organic solvent consumption and improve the extraction time due to the possibility of working at elevated temperatures or pressures in inert atmospheres. A 87 thorough literature search did not yield any reference or reports on the optimization of 88 89 microwave procedure for extraction of phenolic compounds from C. Sinensis peels. Response 90 surface methodology (RSM) is a useful tool to evaluate the effects of multiple factors and 91 their interactions on one or more response variables such as phenolic compounds. The central 92 composite design (CCD) is a popular form of RSM and has been applied by a number of 93 researchers for optimization of various food processing methods such as extrusion cooking (Nayak, Berrios, Powers, & Tang, 2011) and extraction (Huang, Ou, Hampsch-Woodill, 94 95 Flanagan, & Prior, 2002). In this project, we investigated (i) the effects of different extraction 96 parameters on the efficiency and recovery of phenolic compounds from C. Sinensis peels; (ii) 97 RSM technique to optimize microwave-assisted extraction parameters such as microwave power, extraction time, solvent-to- solid ratio to maximize the total phenolic content ; (iii) 98 individual phenolic acids of microwave-assisted (MAE), ultrasound-assisted (UAE), 99 100 accelerated-solvent (ASE) and conventional solvent (CSE) extracted samples. Finally, the 101 total phenolic contents and antioxidant activities (using DPPH radical scavenging assay and 102 ORAC-values) of citrus peels in optimized MAE conditions were compared with UAE, ASE 103 and CSE to understand the most efficient extraction method.

104 2. Materials and methods

105 *2.1 Plant material*

106 The fruit samples of *C. Sinensis* were collected in the area of Oued Ghir (Bejaia, Algeria).

- 107 Samples were washed with distilled water and peeled off manually. Peels were dried in a
- 108 forced-oven at 40 °C to constant weight, and then grounded using an electrical grinder (IKA

109	model- A11, Staufen, Baden-Württemberg, Germany). The ground powder was passed
110	through a standard 125 μm sieve and only the fraction with particle size $<125~\mu m$ was
111	collected and stored at 4 $^{\circ}$ C in airtight bags until further use. The water activity (a _w) of the
112	sample was measured with a HygroPalm AW1 portable water activity meter, (Rotronic,
113	Bassersdorf, Switzerland) and found to be 0.18 ± 0.02 at 20.6 °C.
114	2.2 Reagents
115	Sodium carbonate (Na ₂ CO ₃), Folin-Ciocalteu's phenol reagent and hydrochloric acid
116	(HCl) were purchased from Prolabo (Loire, France). Fluorescein (FL) and Trolox (6-
117	hydroxy-2,5,7,8-tetramethylchroman-2-carboxylic acid), DPPH (1, 1-diphenyl-2-
118	picrylhydrazyl) were purchased from Sigma-Aldrich Co. (St. Louis, MO). HPLC standards
119	such as gallic acid, ferulic acid, caffeic acid, p-coumaric acid, chlorogenic acid, rutin,
120	quercetin, catechin and epigallocatechin were purchased from Fisher scientific (Fair Lawn,
121	NJ, USA). 2-2'-azobis (2-amino-propane) dihydrochloride (AAPH) was purchased from
122	Wako chemicals (Richmond, VA, USA). All the solvents used for extraction and HPLC
123	analysis were HPLC grade.
124	2.3 Extraction and quantification of total phenolic content (TPC)
125	2.3.1 Microwave assisted extraction (MAE).
126	A domestic microwave oven (Samsung model: NN-S674MF, Kuala Lumpur, Malaysia) with
127	cavity dimensions of 22.5 \times 37.5 \times 38.6 cm and a working frequency of 2.45 GHz was used
128	for extraction of phenolic compounds from C. Sinensis peel powders. The apparatus was
129	equipped with a digital control system for measuring extraction time and microwave power
130	(the latter was linearly adjustable from 200 to 1000 W). The oven was modified in order to
131	condense the vapors generated during extraction of the sample. Aqueous acetone in different
132	concentrations was used as a safe and efficient solvent for the extraction of phenolic
133	compounds (Li, Deng, Wu, Liu, Loewen, & Tsao, 2012). The use of acetone allows an

efficient and more reproducible extraction, avoids problems with pectins such as its clotting

135	properties, and permits a much lower temperature for sample concentration Garcia-Viguera,
136	Zafrilla, and Tomas-Barberan (1998).
137	One gram of C. Sinensis peel powder was mixed with aqueous acetone by stirring in
138	preparation for extraction using the MAE system. The MAE extraction parameters were
139	microwave power (300-600 W), extraction time (90–240 s), solvent-to-solid ratio (15-30 mL
140	g^{-1}) and acetone in water concentration (20-80 %, v/v), where the influence of each
141	parameter was investigated in single-factor experiments (Supplement Table S1). Each trial
142	was carried out in triplicate. The temperature of the samples were never exceeded 80 °C
143	during 122 s of extraction at 500 W (optimal conditions). After MAE treatment, the extract
144	was filtered through a Whatman No. 1 filter paper lined in a Büchner funnel and the
145	supernatant was collected in a volumetric flask. The extract was stored at 4 °C until further
146	use. Influence of each factor on the yield of total phenolic content was statistically assessed
147	by ANOVA and Tukey's post-hoc test.

148 2.3.1.1 Experimental Design and Statistical Analyses.

134

149 The influence of the process parameters i.e. type of solvent, microwave power, 150 extraction time and solvent-to-solid ratio were investigated using a single-factor-test to 151 determinate the preliminary range of extraction variables (Supplement Table S1). Based on 152 the single-factor experimental results, major factors influencing the extraction process were 153 selected for designing experiments using response surface methodology (RSM). Minitab 154 statistical software (Minitab, version 8.0.7.1, State college, PA, USA) package was used to 155 establish a mathematical model and obtain the optimum conditions for maximum recovery of 156 TPC. In the present study, a three-level four-factorial Box-Behnken experimental design 157 (BBD) was applied to investigate and validate extraction process parameters affecting the rate 158 of phenolic compounds from C. sinensis peels. The number of experiments (N) required for

159	the development of BBD is defined in Eq.(1) (Dahmoune, Boulekbache, Moussi, Aoun,
160	Spigno, & Madani, 2013).
161	$N = 2k(k-1) + C_0 $ (1)
162	where k is number of factors and C_0 is the number of center points. The factor levels were
163	coded as -1 (low), 0 (center point or middle) and 1 (high), respectively. The four factors
164	chosen for this study designated as X_1 : aqueous acetone (40-60%), X_2 : extraction time (90-
165	150 s), $X_{3:}$ microwave power (400-600 w) and X_4 : solvent-to-solid ratio (20-30 mL g ⁻¹)
166	(Table 1). The variables were coded according to equation Eq.(2) (Dahmoune, Nayak,
167	Moussi, Remini, & Madani, 2015).
168	$x_i = \frac{(X_i - X_0)}{\Delta X} \tag{2}$
169	Where x_i the (dimensionless) coded value of the variable is X_i and X_0 is the value of X at the
170	center point and ΔX is the step change.
171	The experiments were performed according to the design of experiments shown in
172	Table 1. The output results (TPC yield) were fitted to a second-order polynomial equation
173	(quadratic model), according to the model in Eq.(3).
174	$Y = B_0 + \sum_{i=1}^{k} B_i X_i + \sum_{i=1}^{k} B_{ii} X^2 + \sum_{i>j}^{k} B_{ij} X_i X_j + E $ (3)
175	where Y represents the response function (in our case the TPC yield); B_0 is a constant
176	coefficient; B_{i} , B_{ii} and B_{ij} are the coefficients of the linear, quadratic and interactive terms,
177	respectively, and X_i and X_j represent the actual independent variables. The regression

178 coefficients of individual linear, quadratic and interaction terms were determined using

analysis of variance. In order to visualize the relationship between the response and

180 experimental levels of each factor and to deduce the optimum conditions, the regression

181 coefficients were used to generate *3-D* surface plots from the fitted polynomial equation.

182 Analysis of variance (ANOVA) was performed for response variable using the full 183 models where p-values (partitioned into linear and interaction factors) indicated whether the 184 terms were significant or not. To verify the adequacy of the models, additional extraction trials were carried out at the predicted optimal conditions and the experimental data were 185 186 compared to the values predicted by the regression model. Microwave extraction method was 187 compared with UAE, ASE and CSE based on the TPC, antioxidant activity (DPPH assay and 188 ORAC-values) and HPLC results.

189

Ultrasound assisted extraction (UAE) 2.3.2

An ultrasonic system with working frequency fixed at 20 kHz (SONICS Vibra cell, 190 191 VCX 130 PB, stepped microtips and probes, No. 630-0422, Newtown, Connecticut, USA) 192 was used for extraction of phenolic compounds from the citrus peel under optimal conditions 193 (Dahmoune, Moussi, Remini, Belbahi, Aoun, Spigno, et al., 2014). Briefly, 1 g of peel 194 powder was mixed with 50 mL of 75.79 % acetone concentration in a 250 mL amber glass 195 bottle ($\emptyset \times H$: 45 \times 140 mm and cap size of 28 mm) the obtained suspension was exposed to 196 acoustic waves for 8.33 min extraction time, and 65.94% extraction amplitude. The 197 temperature $(27 \pm 2 \text{ °C})$ was controlled continuously by circulating cold water using an 198 external cold-water bath and checking the temperature using a T-type thermocouple 199 (Cooking, Thermo-Timer, China). After the UAE treatment, the supernatant was recovered 200 and analyzed as reported in Section 2.3.1 for the optimized MAE extract.

201

2.3.3 Accelerated solvent extraction (ASE)

202 An accelerated solvent extractor (ASE, Dionex Corp., Sunnyvale, CA) system was 203 used for extraction of phenolic compounds from C. Sinensis following our in-house 204 procedure. Briefly, one gram of peel powder was placed in two layers of diatomaceous earth 205 (about 0.5 g in each layer) in 11 mL Dionex (ASE 200) stainless-steel cell, and phenolic 206 compounds were extracted with 50% acetone. The cells were equipped with a stainless steel

frit and a cellulose filter (Dionex Corp.) at the bottom to avoid the collection of suspended particles in the collection vial. A dispersing agent (diatomaceous earth), was used to reduce the solvent volume. The extraction was performed at 1500 psi and temperature of 120 °C, and then heated for 6 min, followed by three static periods of 5 min (3 static cycles). The sample was flushed with 70% nitrogen for 90 s. Extracts were collected into 50 mL tubes.

212 2.3.4 Conventional solvent extraction (CSE)

Phenolic compounds in citrus peels were extracted using a conventional solvent 213 214 extraction method following the procedures recommended by (Giorgia Spigno, Tramelli, and 215 De Faveri, 2007). Briefly, one gram of powder was mixed with 50 mL of 50% aqueous 216 acetone (v/v) in a conical flask ($\emptyset \times H$: 51 × 150 mm and cap size of 38 mm); the mixture 217 was kept in a thermostatic water bath (model: WNB22, Memmert, Frankfurt, Germany) at 60 218 °C for 2 hours shaking at a speed of 110 strokes per minute. After the CSE treatment, the 219 supernatant was recovered and analyzed as reported in Section 2.3.1 for the optimized MAE 220 extract.

221 2.4 Determination of total phenolic content (TPC)

222 The total phenolic content in the *Citrus sinensis* powder extracts was determined by 223 the Folin-Ciocalteau method (Jaramillo-Flores, González-Cruz, Cornejo-Mazón, Dorantes-224 Alvarez, Gutiérrez-López, & Hernández-Sánchez, 2003). Briefly, twenty micro- Liter of 225 supernatant was mixed with 150 µL of a 10-fold diluted Folin–Ciocalteau reagent. The 226 solutions were mixed thoroughly and incubated at room temperature (27 °C) for 5 min. After 227 incubation, 150 μ L of 6 % sodium carbonate (Na₂CO₃) solution was added and again 228 incubated at 25 °C for 90 min. The absorbance of the reaction mixtures were measured at 725 229 nm using a Omega FLUOstar plate reader (Model : SpectroScan 50, Nicosia, Cyprus). The 230 absorbance of the extract was compared with a gallic acid standard curve for estimating

concentration of TPC in the sample. The TPC was expressed as mg of gallic acid equivalents

- 232 (GAE) per gram of powder on dry weight (DW) basis.
- 233 2.5 Determination of antioxidant activity
- 234 2.5.1 DPPH radical scavenging assay
- The electron donation ability of the obtained acetone extracts was measured by
- bleaching of the purple-colored solution of 1,1-diphenyl-2-picrylhydrazyl radical (DPPH)
- following the procedures of Brand-Williams, Cuvelier, and Berset (1995) with modifications.
- 238 Briefly, 300 μ L of DPPH' solution prepared in methanol (70 μ M) was mixed with 10 μ L of
- 239 peel extracts and the mixture was incubated at 37 °C. The tests were performed on a micro-
- 240 plate reader (Omega FLUOstar, BMG Labtech, Cary, NC, USA). Absorbance readings of the
- 241 mixture were taken at 515 nm over a period of 20 min.
- 242 The antioxidant activity was expressed as percentage of inhibition of DPPH radical
- calculated according to Eq.(4).

244 % inhibition =
$$\frac{A_{blank \ t=20 \ \text{min}} - A_{sample \ t=20 \ \text{min}}}{A_{DPPH \ t=0 \ \text{min}}} \times 100$$
(4)

where A_{blank} is the absorbance value of the blank (300 µL of DPPH solution plus 10 µL of the solvent in which extract has been dissolved); A_{sample} is the absorbance of the sample extract; *t* is the time (min) at which absorbance was read and A_{DPPH} is the absorbance of the control at time = 0 min. The effective concentration of sample required to scavenge DPPH radical by 50% (*IC*₅₀ value) was obtained by linear regression analysis of dose-response curve plotting between % inhibition and concentrations.

251 2.5.2 Oxygen radical absorbance capacity (ORAC) assay

The antioxidant activity of peel extracts were also assessed using an ORAC assay following the procedures of Huang, Ou, Hampsch-Woodill, Flanagan, and Prior (2002) with modifications. Briefly, a stock fluorescein solution (Stock #1) was prepared by dissolving

255 0.0225 g of fluorescein in 50 mL of 0.075 M phosphate buffer (pH 7.0). A second stock 256 solution was prepared by diluting 50 μ L of stock solution #1 in 10 mL of phosphate buffer. 257 An aliquot of 800 µL of solution #2 was added to 50 mL of phosphate buffer, mixed on 258 magnetic stir plate and aliquots were dispensed to 10 mL tubes and placed in 37 °C heating block until the start of the assay. AAPH was used as a peroxyl generator and trolox as a 259 standard. Twenty microliters of sample, blank, and trolox calibration solutions were 260 261 transferred to 96-well microplates in triplicate on the basis of a set layout. The ORAC assays were carried out on Omega FLUOstar plate reader which was equipped with an incubator and 262 two injection pumps. The temperature of the incubator was set to 37 °C. The plate reader was 263 264 programmed to record the fluorescence of fluorescein during each cycle for 40 min. Four 265 calibration solutions of trolox (6.5, 12, 25, 50 µM final concentration) was also tested to 266 establish a standard curve. All samples were analyzed in triplicate. 267 The area under the curve (AUC) was calculated for each sample by integrating the

relative fluorescence curve (Eq.(5)).

269
$$AUC = \left(0.5 + \frac{f_4}{f_3} + \frac{f_5}{f_3} + \frac{f_6}{f_3} + \dots + \frac{f_i}{f_3}\right) \times CT$$
(5)

where f_3 initial fluorescence reading at cycle 3, f_i is a fluorescence reading at cycle *i*, and *CT* is cycle time in minutes. The net *AUC* of the sample was calculated by subtracting the *AUC* of the blank. The regression equation between net *AUC* and Trolox concentrations was determined and ORAC values were expressed as µmol trolox equivalents per gram of sample (µmol TE g⁻¹) using the standard curve established in same condition.

275 2.6 HPLC-DAD analysis

Treated sample and control extracts were fractionated for phenolic acids in four fractions using a SePak C-18 cartridge (Waters, Milford, MA, USA). The columns were activated for neutral phenolics by sequentially passing 50 mL of ethyl acetate, acidified

279 methanol (0.01% v/v HCl) and acidified water (0.01% v/v HCl). Fraction 1 was obtained by 280 eluting 20 ml of crude extract in the column prior to washing the column with 60 ml of 281 acidified distilled water to remove any organic sugars and acids (fraction 2). The retained 282 fraction of phenolic acids was eluted with 60 ml of ethyl acetate (fraction 3). Anthocyanins 283 plus proanthocyanidins (fraction 4) were eluted with 60 ml of acidified methanol. Finally, 284 after evaporation, all fractions (1, 2, 3 and 4) were re-suspended in methanol (HPLC grade) 285 and stored at 4 °C for further analysis. 286 Identification of selected individual phenolic acids was performed using a High-287 Performance Liquid Chromatography (Agilent Technologies, Santa Clara, USA) equipped 288 with a Diode array detector and a column C-18 (5 μ m, 4.60 \times 250 mm, USA). All samples 289 were centrifuged at 5000 rpm for 10 min before injection into the column with an injection

volume of 20 μ L and at a flow rate of 0.5 mL min⁻¹. Chromatographic analysis was carried

out at 30 °C using simultaneous monitoring of extracts performed at 254, 280, 520, 300 and

292 700 nm. The mobile phase A was a mixture of 6:94 (v/v) acetic acid in distilled water,

whereas mobile phase B consisted of 100% HPLC grade acetonitrile. The solvent gradient in

volume ratios was as follows: 0–40 min, 0–25% B; 40–80 min, 25–85% B; 80–90 min, 85–

295 100% B; 90-95 min, 100% B.

290

Individual phenolic compounds were identified based on their elution time and quantified from peak area at 280 nm. Identified phenolic compounds (phenolic acid and flavonoids) were quantified using external standards. The standard response curve was a linear regression fitted to values obtained at each concentration within the range of 12.5–200 μ g mL⁻¹ for phenolic acid (Gallic acid, Ferulic acid, Caffeic acid, *p*-Coumaric acid and Chlorogenic acid) and 41.5-333 μ g mL⁻¹ for flavonoids (Rutin, Quercetin, Catechin and Epigallocatechin).

303 *3 Results and discussion*

304 *3.1 Effects of extraction on the visual color of extracts*

305 Extraction is an important step for the recovery and isolation of bioactive 306 phytochemicals from plant materials before analysis. Liquid-liquid and solid-liquid extraction 307 are the most commonly used procedures prior to analysis of phenolic compounds in natural 308 matrix. They are still the most widely used techniques, mainly because of their efficiency, 309 wide-ranging applicability and ease of use to extract of natural antioxidants. In our study, 310 from the color and turbidity of the acetone-water extracts in relation to the extraction methods 311 i.e. CSE, UAE, MAE and ASE, it was observed that the visual color was influenced by the 312 extraction methods. Most importantly, color of the MAE and ASE extracts turned pale 313 brown, differing from the usual pale green after extraction. In MAE, heat is generated by the 314 volumetric heating of samples with the help of electromagnetic waves; in ASE, high 315 temperature extraction of the samples potentially attributed to the degradation of color 316 compounds. A similar trend in the degradation of color compounds was observed in our 317 previous studies on the extraction of phenolic compounds from C. limon, P. lentiscus and M. 318 communis using MAE, ASE, UAE and CSE (Dahmoune, Boulekbache, Moussi, Aoun, Spigno, & Madani, 2013; Dahmoune, et al., 2014). 319

- 320 *3.2 Modeling of MAE*
- 321

3.2.1 Single factor experiments

Selection of extraction solvents is critical for the complex plant materials as it will determine the amount and type of phenolic compounds being extracted. Aqueous solvents particularly acetone, ethanol and methanol are more commonly used in phenolic extraction from botanical materials than the corresponding mono-component solvent system (Spigno, Tramelli, & De Faveri, 2007). In the present study with preliminary single factor experiments, we observed that the type of solvent significantly influenced the TPC yield

328	during MAE, with 50% aqueous acetone (11.49 \pm 0.44 mg GAE g ⁻¹) providing higher
329	recovery than water (7.63 \pm 1.22 mg GAE g ⁻¹), 50% aqueous ethanol (6.29 \pm 0.77 mg GAE
330	g ⁻¹) and 50% aqueous methanol (9.68 \pm 0.99 mg GAE g ⁻¹) (<i>supplement Table S2</i>). Higher
331	recovery of TPC by aqueous acetone could be attributed to better absorption of microwave
332	energy by the extract during MAE due to volumetric heating. This process increases
333	temperature inside the plant cells, resulting in breaking the cell walls and releasing
334	compounds in to the surrounding solvent. Aqueous acetone was then selected for the RSM
335	trials and for subsequent single-factor trials.
336	The effect of various percentages of acetone in water (20-80%) as an extraction
337	solvent to recover phenolic compounds was investigated. TPC yield increased with increasing
338	aqueous acetone concentration up to 50% and then decreased slightly at higher concentrations
339	(supplement Table S2). Thus, the acquired ratio of TPC increased with decreasing water
340	content following the principles of "like dissolves like" (Zhang, Bi, & Liu, 2007). In the
341	second step, the proportion of acetone in the extraction solvent was varied between 40 and
342	60% for the optimization design. The solvent with 50% acetone content was then chosen for
343	the determination of optimal microwave power, extraction time and solvent-solid ratio.
344	Selection of an appropriate microwave power for extraction was the third step in a
345	series of preliminary experiments. Phenolic compounds were extracted from C. sinensis peel
346	samples by varying the microwave power using 50% aqueous acetone for 120 s while
347	keeping the solvent-to-solid ratio constant at 20 mL g^{-1} . The results showed that the TPC
348	increased when microwave power increased from 400 to 500 W. Beyond 500 W, TPC
349	decreased sharply and reached a minimum at 800 W (Supplement Table S2), possibly due to
350	the degradation of compounds with the higher microwave power during extraction (Proestos
351	& Komaitis, 2008). Based on the preliminary tests, the best microwave power for the

extraction was selected as 500 W. The lower, middle and upper levels of extraction power

chosen for RSM were 400, 500 and 600 W, respectively.

354 Extraction time is another parameter that influences the yield of TPC and should be considered for the optimization procedure. Generally, by increasing the extraction time, the 355 quantity of analytes extracted is increased, although there is a risk that degradation of 356 phenolic compounds may occur (Proestos, Boziaris, Nychas, & Komaitis, 2006). The 357 358 acquired ratio of TPC extraction gradually increased with increasing extraction time and the 359 maximum TPC was obtained between 30-120 s (Supplement Table S2). A significant increase 360 in extraction efficiency was observed as the extraction time increased from 90 to 120 s 361 followed by a significant decrease after 125 s (Supplement Table S2). Longer irradiation 362 exposition without temperature control could have induced thermal degradation of phenolic 363 compounds (Yang, Jiang, Li, Chen, Wang, & Zhu, 2009). Since shorter extraction time is 364 also favorable to reduce energy costs, the 90 - 150 s range was selected for the optimization. 365 The solvent-to-solid ratio can influence the TPC yield. In the present study, solventto-solid ratio was set at 15:1, 20:1, 25:1 and 30:1 (mL g^{-1}) respectively. It was observed that 366 the extraction yield increased quickly with the increase of solvent-solid ratio from 15:1 - 25:1367 mL g⁻¹ (Supplement Table S2). Then, extraction yield rapidly decreased with increase in 368 solvent /material ratio from $25:1 - 30:1 \text{ mL g}^{-1}$. The solvent-to-solid ratio significantly 369 370 influenced the TPC yield, showing similar trend on the extraction of tea polyphenols using 371 microwave as reported by Spigno and De Faveri (2009). However, the decrease in the 372 extraction yield beyond a solvent-to-solid ratio could be due to the non-uniform distribution 373 and exposure to microwave heating (Eskilsson & Björklund, 2000). Furthermore, the 374 optimized solvent volume should be sufficient to ensure that the entire sample is immersed, 375 especially when a sample will swell during the extraction process (Dahmoune, Boulekbache,

376 Moussi, Aoun, Spigno, & Madani, 2013; Eskilsson & Björklund, 2000). Based on statistical

analysis, the range 20–30 mL g^{-1} was selected for the RSM optimization.

378 *3.2.2 Optimization of MAE technique*

379 In this study, we evaluated the effects of microwave power, extraction time and 380 solvent-to-solid ratio with the Box-Behnken experimental design. Aqueous acetone was used for all the extraction methods. The data on the yield of TPC obtained from 27-runs of 381 382 experiments using MAE was analyzed using ANOVA and are shown in Table 1. A quadratic 383 model was fitted to the generated data to test the significance and adequacy of the model. From the significant levels obtained at p < 0.001, it was observed that the data adequately fit 384 the developed model (Table 2). In addition, the coefficient of determination ($R^2=0.92$) and 385 adjusted determination coefficient (Adj. $R^2 = 0.89$) were reasonably close to 1, indicating a 386 high degree of correlation between the observed and predicted values. Additionally, a low 387 value of coefficient of the variation (CV = 3.96%) indicated a high degree of precision and a 388 good deal of reliability of the experimental values. 389 390 From the regression equation, it can be observed that the independent variables have a linear effect on the yield of TPC(Y) within the experiment range in MAE. The TPC 391

extraction yield was affected more significantly by acetone concentration at p < 0.001 (p =

393 0.0001), followed by extraction time at p < 0.05 (p = 0.0492), while TPC recovery was not 394 affected (p > 0.05) by other factors, i.e. extraction power (p = 0.4163) and solvent-solid ratio 395 (p = 0.1257). The quadratic terms X_1^2 , X_2^2 , X_3^2 and X_4^2 were highly significant at the level 396 p < 0.001 (Table 2).

The interaction (cross product) of extraction time and solvent-solid ratio (X_2X_4) was statistically significant at p < 0.001 followed by (X_1X_4) at p < 0.05 (Table 2). Neglecting the non-significant terms (p < 0.05), the final predicted second-order polynomial equation obtained is given in Eq.(6)

401	$Y = 12.1567 + 0.4967X_1 - 0.4225X_1X_4 - 0.8675X_2X_4 - 1.7291X_1^2 - 1.2404X_3^2 - 0.9091X_4^2 $ (6)
402	The effects of the independent variables and the mutual interaction on the extraction yield of
403	TPC can also be seen on three dimensional response surface curves shown in Figure 1A–F.
404	Each 3D plot represents the number of combinations of the two-test variable. Figure 1A
405	shows a higher interaction between the solvent-solid ratio and extraction time ($p < 0.001$); the
406	TPC increased roughly from 8.72 to 10.82 mg GAE g^{-1} DW when the ratio was fixed at 20
407	mL g^{-1} and time varies for 90 to 133 s. The decline in TPC was observed after 122 s at a
408	solvent-solid ratio of 25 mL g^{-1} . The TPC yield reach a minimum of 9.25 mg GAE g^{-1} DW
409	at 150 s and at extraction ratio 30 mL g^{-1} .
410	Response surface for TPC yield with varying ratio of solvent to solid samples and
411	aqueous acetone concentration are shown in Figure 1B. Simultaneous increase in the ratio of
412	solvent to solid from 20 to 25 mL g^{-1} and aqueous acetone concentration from 40 to 50%,
413	increased the TPC yields from about 9 to 12.19 mg GAE g^{-1} DW. It was also observed that
414	the extraction yields decreased along with the increase in the ratio of solvent to solid from 25
415	to 30 mL g^{-1} and aqueous acetone concentration of 50 to 60%. The results suggested that the
416	interaction between the ratio of solvent-to-solid and aqueous acetone concentration on the
417	extraction efficiency of TPC was highly significant ($p < 0.01$). Figure 1C shows the effects of
418	aqueous acetone concentration and microwave power on the TPC of the C. sinensis peels. By
419	increasing the microwave power from 436 to 496 W with aqueous acetone concentration
420	fixed at 41% (acetone/water, v/v), the TPC increases from 9.45 to 10.04 mg GAE g^{-1} DW.
421	However, the TPC increases from 9.45 to 12.19 mg GAE g^{-1} DW if the aqueous acetone
422	concentration and microwave power were increased simultaneously until 50% and 500 W
423	respectively. The reduction in the TPC up to a value of 9.72 mg GAE g^{-1} DW was noticed
424	when one exceeds the optimal conditions (beyond 500 W and 50% acetone in water). This
425	was due to the increase in the direct effect of microwave energy on the medium of extraction

426 by the dipolar rotation that resulted in a rise in temperature of the medium and caused the

427 degradation of the bioactives substances (Hayat, et al., 2010).

428 The recovery of TPC was affected with response to the interaction between microwave power and solvent-to-solid ratio, when other factors (extraction time and aqueous 429 acetone proportion) were fixed at 120 s and 50% respectively (Figure 1D). The results 430 431 indicated that TPC yield increased with the increase in microwave power and solvent-solid 432 ratio at the beginning of extraction. The recovery reached its maximum of 12.10 ± 0.15 mg GAE g^{-1} DW at 500 W and a solvent-solid ratio of 25 mL g^{-1} during the MAE process. 433 Increasing the microwave power further to more than 500 W, the extraction recovery of TPC 434 decreased with a solvent-solid ratio of 25 mL g^{-1} . These results are in agreement with those 435 found by Shao, He, Sun, and Zhao (2012), who observed that a strong microwave power 436 437 leads to an increase in the temperature, which negatively affects the thermo-labile 438 compounds. Figure 1E shows the profiles obtained on the effects of the aqueous acetone 439 concentration and extraction time on the yield of TPC. An increase in the TPC yield was 440 observed with the increase in aqueous acetone concentration and extraction time, but the tendency was reversed when the interaction between solvent-solid ratio and extraction time 441 442 reached a certain value. A few seconds of peel exposure to microwave showed an excellent 443 yield in TPC, but longer duration enhanced the degradation of the thermo-labile compounds. Figure 1F shows that increase in extraction time and microwave power increased the TPC up 444 to a maximum of 12 mg GAE g^{-1} DW. However, a prolonged extraction time with the 445 446 microwave power gave reduced TPC yield, which was also noticed during our preliminary 447 study.

448 Under the optimal conditions of microwave power, extraction time, aqueous acetone 449 concentration and solvent-solid ratio, the model predicted a maximum response of 12.20 mg 450 GAE g^{-1} DW. To compare the predicted results with the experimental values, rechecking

451 was performed using this deduced optimal condition. It led to an experimental yield of TPC 452 equal to 12.09 ± 0.06 mg GAE g⁻¹ DW, which is close to the predicted value (12.20 mg GAE 453 g⁻¹ DW). The best correlation between these results confirmed that the response model was 454 adequate, and valid enough to reflect the expected optimization results (*Supplement Table* 455 *S3*).

456

3.3 Comparison of extraction methods on recovery of TPC

457 To evaluate the efficiency of extraction and validate the MAE procedure for 458 polyphenol-rich extract, C. sinensis peels were extracted and compared with CSE, UAE and 459 ASE. Recovery of the TPC in extracts were compared using the above selected extraction 460 methods (Table 3). The results of the MAE experiments indicated that microwave assistance 461 enhanced the efficiency of yield of TPC significantly (p < 0.01) compared to UAE, CSE and 462 ASE. Higher yield of TPC in MAE could be attributed to the microwaves ability to penetrate 463 cell matrix and interact with polar molecules resulting in volumetric heating of biomaterial, 464 consequently leading to a pressure increase inside the plant cell. This pressure increase leads 465 to breaking of cell walls and release of phenolic analytes. Besides, breakdown of bigger 466 phenolic compounds into smaller ones with their intact properties of the original molecules, 467 as measured by Folin-Ciocalteau assay, could have provided the higher yield TPC (Nayak, 468 Liu & Tang, 2015). However, this observation was in contrary to Pingret (2012, 2013), who 469 reported degradation of bioactive compounds by microwave and ultrasound waves. The lower 470 TPC in the ASE treatments using aqueous acetone at 120 °C may be due to the breakdown of 471 phenolic compounds that were not detected using Folin-Ciocalteau assay. In addition, 472 combined effects of oxidation during the extraction process and of non-phenolic compounds 473 such as sugar, fatty acids interaction with the phenolic compounds might have lowered the 474 TPC in ASE extracts and the recovery might have underestimated since the extract showed 475 the dark color.

476 *3.4 Effects of extraction methods on the antioxidant activity*

477	The antioxidant activities of C. Sinensis extracts were evaluated by DPPH radical
478	scavenging assay and ORAC test. The reduction of the DPPH absorbance at 517 nm after 20
479	min incubation was measured with different concentrations of the extract (Figure 2). Extracts
480	from MAE showed lower IC_{50} (337.16 ± 8.45 ml extract L ⁻¹) compared to other extraction
481	methods ($p < 0.05$), indicating that significantly higher antioxidant activities of MAE with
482	higher scavenging of DPPH radicals compared to UAE (IC_{50} : 437.45 ± 1.30 ml extract L ⁻¹),
483	CSE (IC_{50} : 357.36 ± 6.02 ml extract L ⁻¹) and ASE (IC_{50} : 450.44 ± 4.48 ml extract L ⁻¹)
484	methods (Table 3). The higher activity of MAE extract could be explained by microwave
485	treatment that affects the structure of the cell due to the sudden increase in temperature and
486	internal pressure; which can be observed clearly under scanning electron microscope
487	(Dahmoune, Boulekbache, Moussi, Aoun, Spigno, & Madani, 2013; Dahmoune, Nayak,
488	Moussi, Remini, & Madani, 2015). The principle of volumetric heating using microwave
489	energy is based on the direct effect of microwaves on molecules by ionic conduction and
490	dipole rotation. This results in rapid rise of the temperature and fast completion of a reaction.
491	Although ultrasound can break the cell wall with its cavitation power, releasing phenolic
492	compounds into the extraction solvent, the quantity of release depends on the intensity and
493	duration of application. In our study, the ultrasound parameters selected for treatment and
494	extraction duration produced lower recovery of total phenolics and hence less antioxidant
495	activity.

Using the ORAC assay, it was observed that antioxidant activities of extracts were statistically similar for MAE, UAE and CSE, but higher (p < 0.05) compared to the ASE (Table 3). The antioxidant activity of peel extracts using ASE was 337.97 ± 23.15 µmol TE g^{-1} . It was observed that ASE-extracts had the lowest fluorescence intensity during the test compared to other extraction methods. As noticed, the fluorescence signal declined

501	dramatically in the	presence of a peroxy	l generator	(AAPH) beyond	15 min whereas in MAE,
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502 UAE and CSE-extracts the tendency was prolonged until 30 min. This mechanism in ASE

503 extracts could explain the lowest antioxidant activity in the sample extracts (Figure S1).

504 *3.5 HPLC-DAD analysis*

505 The identification and quantification of individual phenolic compounds of C. sinensis extracts 506 was based on a combination of retention times and calibration curve of external standards using a reverse phase C_{18} column in HPLC. The peaks of the phenolic compounds were 507 detected at a wavelength of 280 nm. The elution times of gallic acid, chlrogenic acid, caffeic 508 acid, ferulic acid, p-coumaric acid were 8.7, 23.5, 27.1, 39.5 and 58.6 min, respectively. 509 510 Similarly, elution times of catechin, rutin and quercitin were 20.5, 38 and 54.5 min, 511 respectively (Dahmoune, Nayak, Moussi, Remini, & Madani, 2015). None of the extraction 512 methods provide a particular trend of quantity of phenolic compounds in the extract. While the quantity of chlorogenic acid (1535 $\mu g g^{-1}$ DW), catechin (3037 $\mu g g^{-1}$ DW) and rutin 513 (1253 μ g g⁻¹ DW) were highest, gallic acid (85 μ g g⁻¹ DW) was lowest in CSE extracts 514 515 compared to other extraction methods (Table 4) (Hayat, et al., 2010). Quercitin was not detected in any of the extracts. UAE provided higher recovery of gallic acid (210 μ g g⁻¹ DW) 516 and p-coumaric acid (171 μ g g⁻¹ DW) than other methods (Table 4). Recovery of caffeic acid 517 (815 μ g g⁻¹ DW) and ferulic acid (1455 μ g g⁻¹DW) was highest in MAE extracts (Figure 3) 518 519 compared to UAE, CSE and ASE (figures S2, S3 and S4 in supplemental). From the recovery 520 of individual phenolic compounds using HPLC, it can be reported that CSE, MAE, UAE and 521 ASE favor particular types of phenolic compounds. For example, MAE and ASE may have 522 produced a harsh extraction condition for gallic acid; ultrasound could have a conducive 523 environment whereas type or longer duration of extraction in CSE could have reduced the 524 recovery of gallic acid. Overall, CSE followed by MAE provided the highest quantity of the

total of the selected individual phenolic compounds. In addition, a number of other phenolicacids were also detected in the extracts that were not identified.

527 The results of this study contributed to lighten ways of valorization of the Citrus sinensis peels based on the "six principles of Green Extraction of Natural Products" as 528 outlined by Chemat, Vian, and Cravotto (2012). Some of the major findings from this 529 530 investigation support the idea of green extraction. For example, (i) reduction in the 531 processing time (122, 500, 900 and 7200s for MAE, UAE, ASE and CSE, respectively), (ii) 532 reduction in the extraction solvent consumption, (iii) higher extraction recovery of TPC (at 533 the lab-scale batch process, the yield of TPC was 356.75, 305.41, 184.72 and 301.27 Kg $ton^{-1} h^{-1}$ for MAE, UAE, ASE and CSE, respectively), (iv) in the case of MAE, microwaves 534 535 are selectively absorbed by the residual water present in *Citrus Sinensis* peels (about 68 % of 536 moisture), and (v) possible customer acceptance of the by-products (peels) made through this 537 MAE "cleaner, greener" extraction technology.

538 Industrialization of the proposed techniques can be possible by experimental 539 validation and scaling up of the lab parameters in terms of extraction time, yield, chemical 540 composition and quality of environmentally friendly bioactive compounds to a pilot scale. 541 Small scale-up of extraction techniques have been reported for MAE (Petigny et al., 2014), 542 UAE (Achat et al., 2012) and ASE techniques in the literature. There are few reports 543 available on the use of MAE (Zhang, Yang, & Wang, 2011, Filly et al., 2014), UAE (Virot et 544 al., 2010) and ASE (Rabhi et. al., 2015) in the large-scale industrial processing of plant 545 secondary metabolites.

546 *4* Conclusion

547 While almost all of the agricultural and food industries are looking for products processed 548 from pulp or flesh of fruits and vegetables, few have put forth the effort to understand and 549 produce value-added products from downstream by-products. Extraction and standardization

550 of valuable bioactive phytochemicals are important to obtain most of their value by-products. 551 Innovative technology assisted extractions tremendously reduce the extraction time. They 552 have also been shown to use less extraction solvent for a particular bioactive phytochemical 553 when conditions are optimized. The use of mathematical models can be an option to replace 554 conventional extraction methods, providing optimal and predictable results when coupled 555 with MAE. In our study, it was observed that *Citrus sinensis* peels are rich in phytochemicals 556 with antioxidant activity. We established an improved and optimized procedure for extracting 557 polyphenols from C. sinensis peels using MAE method. It was found that MAE not only 558 provided higher recovery of TPC, but also quality phenolic compounds with rich antioxidant 559 activity. In comparison of MAE with CSE, UAE and ASE extracts, it was observed that the 560 mechanism of each extraction i.e. application of microwave or ultrasound or accelerated 561 solvent has its own effects on selected individual phenolic compounds. Further studies 562 concerning benefits of polyphenols from the C. sinensis peels are required before large scale 563 utilization is recommended. For the industrial application, this research could be a basis for 564 further pilot-scale trials of MAE as a green extraction technology for the recovery of highadded value compounds from biomass residues. 565

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691 **Figure captions**

692 Figure 1. Response surface analysis for the total phenolic yield from *Citrus sinensis* peels

- 693 with microwave assisted extraction with respect to solvent-solid ratio and extraction time (A);
- 694 solvent-solid ratio and acetone concentration (B); microwave power and acetone
- 695 concentration (C); solvent-solid ratio and microwave power (D); extraction time and acetone
- 696 concentration (E); microwave power and extraction time (F).
- 697 Figure 2. Antioxidant activity of *Citrus sinensis* peel extracts by microwave-assisted
- 698 extraction (MAE), conventional solvent extraction (CSE), ultrasound-assisted extraction
- 699 (UAE) and accelerated solvent extraction (ASE) as assessed using % inhibition of DPPH
- radicals. The effective concentration of extracts required to scavenge DPPH radical by 50%
- 701 (IC $_{50}$ value) was obtained by linear regression analysis.
- **Figure 3.** Chromatograms of phenolic acids in different fractions (A: fraction 1; B: fraction
- 2; C: fraction 3; D: fraction 4) of microwave-assisted extracted (MAE) of Citrus sinensis peel
- extracts. Phenolic compound 1: gallic acid; 2: chlorogenic acid; 3: caffeic acid; 4: ferulic
- acid; 5: p-coumaric acid and 6: rutin. Elution times and maximum absorbance of individual
- phenolic acids were determined using a reverse phase C18 column in HPLC. The mobile
- phase A was a mixture of 6:94 (v/v) acetic acid in distilled water and mobile phase B
- consisted of 100% HPLC grade acetonitrile. The solvent gradient in volume ratios was as
- follows: 0–40 min, 0–25% B; 40–80 min, 25–85% B; 80–90 min, 85–100% B; 90-95 min,

710 100% B.

Table 1

Experimental design with the observed responses for the recovery of the TPC from *Citrus sinensis* peels using MAE. The codes (-1, 0, 1) and actual values for X_1 (40, 50, 60), X_2 (90, 120, 150), X_3 (400, 500, 600) and X_4 (20, 25, 30).

Run	X ₁ Acetone Concentration (% v/v)	X ₂ Extraction time (s)	X3 Microwave power (W)	X_4 Solvent- solid ratio (mL g ⁻¹)	Recovery of TPC (mg GAE g ⁻¹ DW)		
	1 (10)	0 (100)	0 (500)		0.00 1.00		
1	-1(40)	0 (120)	0 (500)	-1 (20)	9.99 ± 1.60		
2	-1 (40)	1 (150)	0 (500)	0 (25)	8.83 ± 1.17		
3	0 (50)	1 (150)	1 (600)	0 (25)	10.14 ± 2.07		
4	0 (50)	1 (150)	0 (500)	1 (30)	9.22 ± 1.25		
5	-1(40)	-1 (90)	0 (500)	0 (25)	8.49 ± 1.43		
6	0 (50)	0 (120)	-1 (400)	1 (30)	10.25 ± 1.64		
7	0 (50)	0 (120)	0 (500)	0 (25)	11.57 ± 1.28		
8	0 (50)	-1(90)	-1 (400)	0 (25)	10.31 ± 1.66		
9	-1(40)	0 (120)	1 (600)	0 (25)	9.76 ± 2.30		
10	0 (50)	0 (120)	-1 (400)	-1 (20)	9.65 ± 1.13		
11	0 (50)	0 (120)	1 (600)	1 (30)	10.41 ± 2.84		
12	0 (50)	-1 (90)	0 (500)	1 (30)	10.22 ± 1.79		
13	-1(40)	0 (120)	1 (600)	0 (25)	8.94 ± 1.69		
14	0 (50)	-1 (90)	1 (600)	0 (25)	8.82 ± 2.07		
15	-1(40)	1 (150)	0 (500)	0 (25)	9.92 ± 1.55		
16	-1(40)	0 (120)	0 (500)	1 (30)	9.25 ± 1.58		
17	-1(40)	0 (120)	-1 (400)	0 (25)	10.29 ± 1.39		
18	0 (50)	1 (150)	-1 (400)	0 (25)	10.57 ± 1.26		
19	-1(40)	0 (120)	0 (500)	-1 (20)	8.54 ± 2.36		
20	0 (50)	-1(90)	0 (500)	-1 (20)	8.33 ± 1.36		
21	-1(40)	0 (120)	-1 (400)	0 (25)	8.66 ± 2.93		
22	0 (50)	1 (150)	0 (500)	-1 (20)	10.8 ± 2.45		
23	0 (50)	0 (120)	0 (500)	0 (25)	11.81 ± 1.28		
24	0 (50)	0 (120)	1 (600)	-1 (20)	9.62 ± 2.05		
25	-1(40)	0(120)	0 (500)	1 (30)	9.49 ± 2.24		
26	-1(40)	-1(90)	0 (500)	0(25)	9.70 ± 1.89		
27	0 (50)	0 (120)	0 (500)	0 (25)	12.09 ± 1.71		

GAE: gallic acid equivalents ; TPC : total phenolic contents ; MAE : microwave-assisted extraction.

Table 2

Analysis of variance (ANOVA) for the effects of acetone concentration, microwave power, extraction time and solvent-solid ratio on TPC of *Citrus sinensis* peels.

Parameter	Estimated coefficients	Standard error	F- value	Prob > <i>F</i>
Model			26.49	< 0.0001
Intercept				
B_0	12.1566	0.2062	58.94	<0.0001***
Linear				
X_1	0.4966	0.1031	4.82	0.0001***
X_{2}	0.2175	0.1031	2.11	0.0492*
Quadratic				
X_1^2	-1.7291	0.1568	-11.18	<0.0001***
X_2^2	-1.1679	0.1568	-7.55	< 0.0001***
X_{3}^{2}	-0.9091	0.1568	-5.88	0.0001***
Interaction				
$X_1 X_4$	-0.4225	0.1786	-2.36	0.0294*
$X_2 X_4$	-0.8675	0.1786	-4.86	0.0001**
Lack of fit			0.24	0.9629
R^2			0.92	
$Adj R^2$			0.89	
C.V. %			3.96	
KNISE			0.55	

* p < 0.05; ** p < 0.01; *** p < 0.001; **TPC**: total phenolic content; X_I : Acetone concentration (% v/v); X_2 : Extraction time (s); X_3 : Microwave power (W); X_4 : Solvent-solid ratio (mL.g⁻¹).

Table 3

Comparison of the TPC and antioxidant activity (using DPPH radical scavenging asssay and ORAC-values) of *Citrus sinensis* peels using extraction methods of MAE, UAE, ASE and CSE. Results are expressed as means \pm standard deviation.

Extraction methods	TPC (mg GAE g ⁻¹ DW)	DPPH (IC ₅₀ , mL extract L ⁻¹)	ORAC of extract (µM TE g ⁻¹)		
MAE	12.09 ± 0.06^{a}	$337.162 \pm 8.45^{\circ}$	482.27 ± 57.43^{a}		
UAE	10.35 ± 0.04^{b}	433.084 ± 7.62^{a}	456.94 ± 35.09^{a}		
ASE	$6.26\pm0.23^{\rm c}$	450.443 ± 9.49^{a}	337.97 ± 23.15^{b}		
CSE	10.21 ± 0.01^{b}	358.456 ± 5.15^{b}	523.04 ± 48.16^{a}		

Same letters in the same column refer to means not statistically different according to ANOVA and Tukey's test; **TPC**: total phenolic content, **GAE**: gallic acid equivalents; **DW** : dry weight; **TE** : trolox equivalent ; **MAE** : microwave-assisted extraction ; **UAE** : ultrasound-assisted extraction ; **ASE** :accelerated solvent extraction ; **CSE** : conventional solvent extraction.

	Extraction methods	Gallic acid	Chlorogenic acid	Caffeic acid	<i>p-</i> coumaric acid	Ferulic acid	rutin	Quercetin	Catechin	SPC
Fraction 1*	CSE	ND	216.34	59.29	ND	ND	ND	ND	ND	275.64
	MAE	ND	210.12	62.52	ND	ND	ND	ND	ND	272.64
	UAE	64.85	455.46	127.82	ND	17.12	ND	ND	ND	648.14
	ASE	44.20	187.55	59.30	ND	ND	ND	ND	ND	291.06
Fraction 2**	CSE	85.28	796.41	192.07	ND	ND	ND	ND	201.45	1275.21
	MAE	142.69	679.12	166.38	ND	ND	ND	ND	ND	988.20
	UAE	145.80	837.06	47.62	ND	ND	ND	ND	521.47	1551.95
	ASE	70.81	315.41	80.01	ND	ND	ND	ND	ND	466.24
Fraction 3**	CSE	ND	109.42	284.69	5.08	1227	161.09	ND	ND	1787.27
	MAE	ND	273.92	417.11	23.66	1356	199.57	ND	533.91	2270.6
	UAE	ND	74.83	197.85	5.54	623	74.54	ND	ND	976.51
	ASE	ND	253.46	174.98	ND	ND	ND	ND	ND	428.45
Fraction 4**	CSE	ND	413.61	235.50	41.05	ND	1092.66	ND	2836.06	4618.89
	MAE	ND	224.97	169.93	101.28	99.22	389.56	ND	1969.69	2954.65
	UAE	ND	74.84	130.07	165.93	128.27	908.24	ND	463.06	1870.43
	ASE	ND	366.47	221.07	30.71	327.91	1155.51	ND	ND	2101.68
Total	CSE	85.28	1535.78	771.55	46.14	1227	1253.75	ND	3037.51	7957.02
	MAE	142.69	1388.13	815.95	124.95	1455	589.13	ND	2503.60	7020.01
	UAE	210.65	1442.19	503.36	171.47	769	982.79	ND	984.54	5064.15
	ASE	115.01	1122.91	535.38	30.71	327.91	1155.51	ND	ND	3287.44

Table 4 Quantity of selected individual phenolic compounds ($\mu g g^{-1} DW$) in CSE, MAE, UAE and ASE *Citrus sinensis* peel extracts.

SPC: sum of individual phenolic content; ND: Not Detected; *: the fraction eluted from the crude extract; **: Fractions 2, 3 and 4 obtained from elution with acidified distilled water, ethyl acetate and acidified methanol, respectively.

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-5

90 100

Retention time (min)

SCI

Retention time (min)

Highlights

- RSM was applied to optimize TPC extraction from C. sinensis peels using MAE. •
- MAE method was optimized and compared to UAE, CSE and ASE in term of TPC. ٠
- Antioxidant activity of peels using DPPH and ORAC methods retained in MAE. •
- Individual phenolic compounds identified in four fractions of peel extracts. •

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